



#### Getting The Most Out Of Sludge

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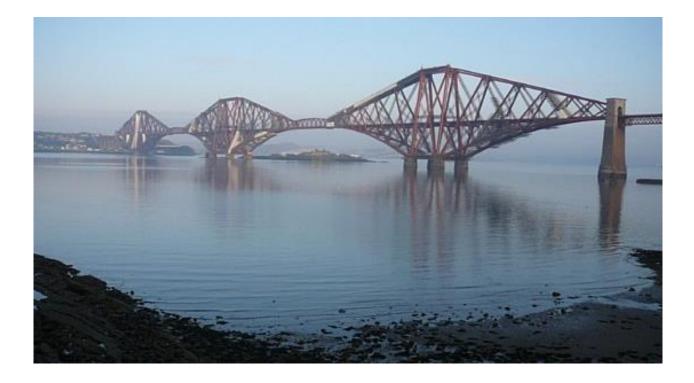
#### The largest single arch railway bridge:1725



Roman design: unchanged since 179 BC

Causey Arch, Built 1725

## Largest Railway Bridge 1882



- Designed in the 1880s
- Design grounded in sound structural theory of Maxwell and Rankine

#### Sludge and Thermodynamics

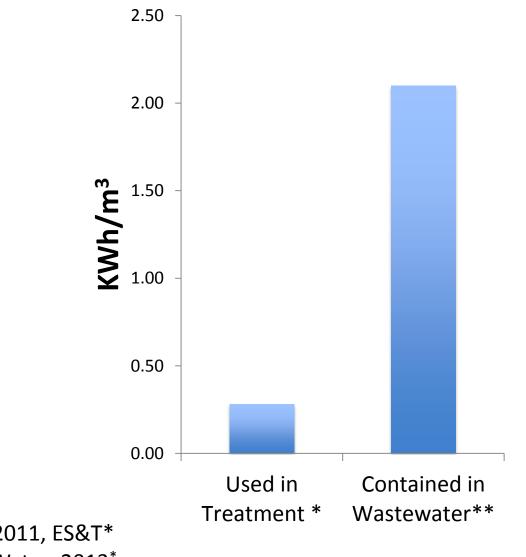
$$-DG_{Cat}$$

$$DG_{Ana} + DG_{dis}$$

 $-\Delta G^{01}_{cat}$  Aerobic Heterotrophs = 2942 (kJ/moleDonor)  $-\Delta G^{01}_{cat}$  Anaerobic Fermenters= 136 (kJ/moleDonor)

#### Sludge is an inevitable consequence of using oxygen as a terminal electron acceptor

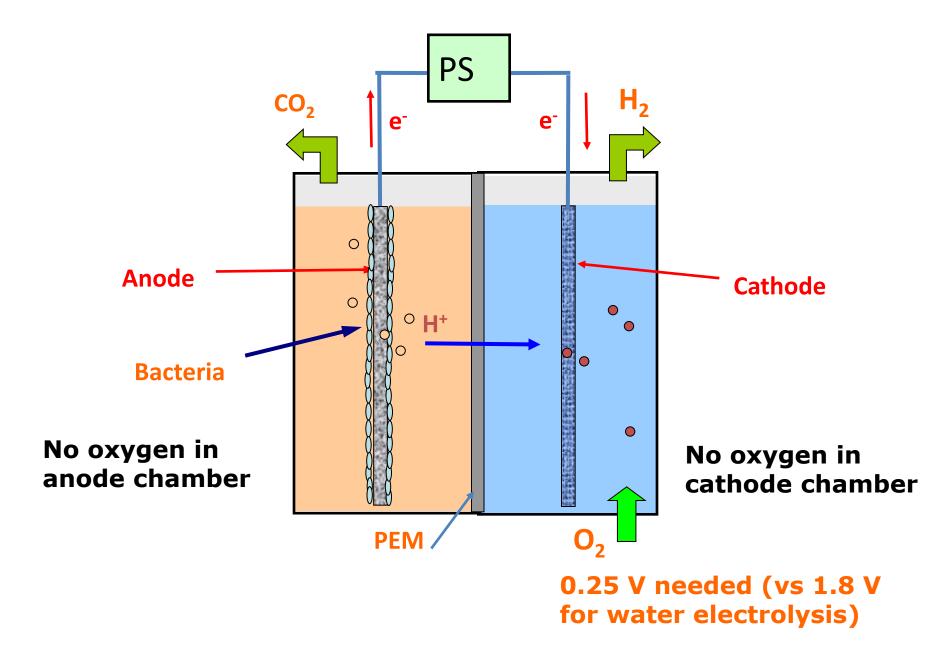
#### Energy in Wastewater: 8Kj/litre



Heidrich et al., 2011, ES&T\* Northumbrian Water 2013<sup>\*</sup> Change Your Electron Acceptor Change Your Thermodynamics

- 1. An Electrode
  - Microbial Electrolysis Cell
- 2. CO<sub>2</sub>
  - Anaerobic Wastewater Treatment

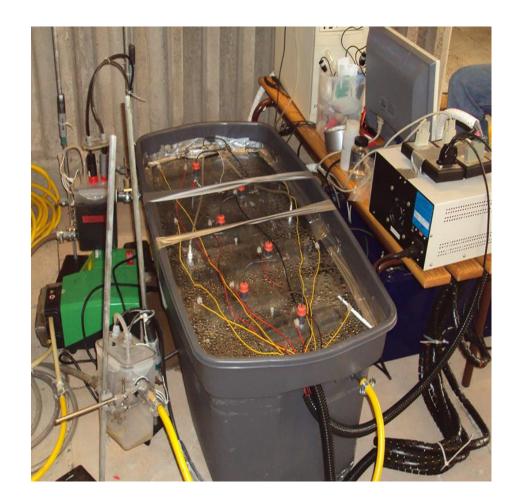
#### Microbial Electrolysis Cell: Make Hydrogen from Sewage





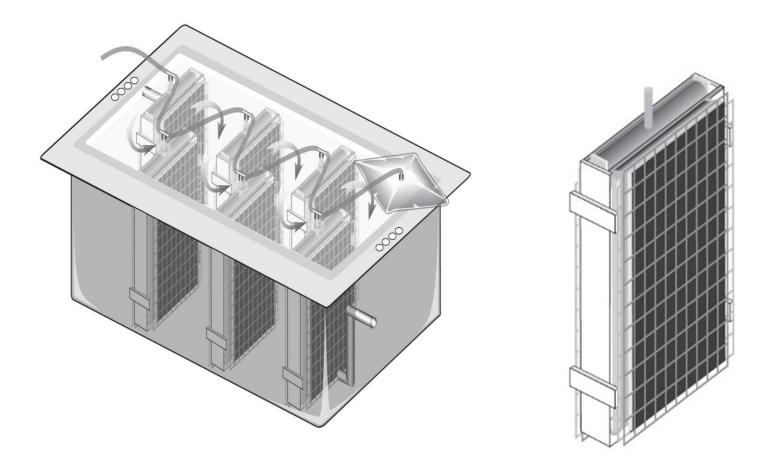
# **Simple Designs**

- Low load
- Low temperatures
- Cheap materials



### But we understood the principles

- Rare electrogenic microbes + low temp = long start up
- Membrane needed (microbes eat H<sub>2</sub>)
- Design simple, low cost, retrofittable, scalable (now 1m<sup>2</sup>)



# And so - it works

- 0.6 L/day of 99% pure hydrogen for 12 months
- Gas production continuous
- Average 50% of the electrical energy input was recovered
- Average COD removal 44%
- Volumetric loading rate was 0.14 kgCOD/m<sup>3</sup>/day,

Heidrich et al. 2013, 2014.

### But it does not pay (yet)

• Longer Reactors for COD removal

• More efficient 3D Anodes

• Improved H<sub>2</sub> recovery

• Break even vs Activated Sludge ~ 5 years

#### Full Scale Domestic Wastewater Treatment in UASB (PE ~1000,000)



Minas Gerais, Brazil

#### UASB in The UK

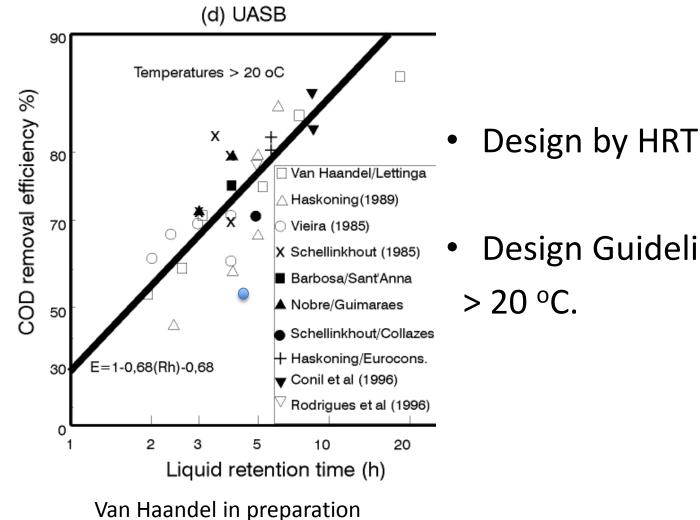
- Great work in Cranfield
  - UASB
  - Membrane Reactors
    - Energy negative

• Struggle at <10°C



Thank you: Bruce Jefferson and Ana Soares

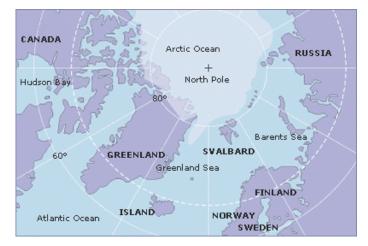
#### **UASB** Key Details: reactor size



Design Guidelines all at

#### Looking For Low Temperature Anaerobes

Svalbard, in the high Arctic "N78°, E11, 15,16°" (average temperature -16 – 6 °C)







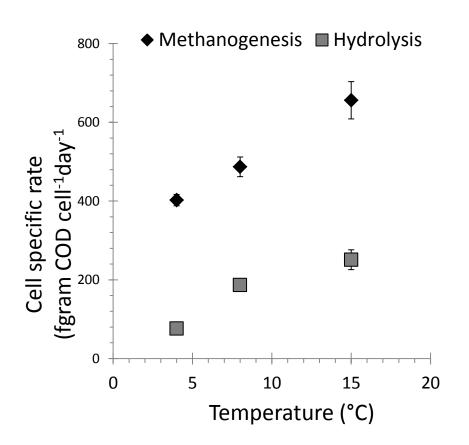
Lake Geneva "N 46°23'04", E 6°25'07" (average temperature -11 – 17 °C)





### Activity Down to 4°C

- Totally Different Bacteria
- COD Removal < 100 mg/l at 4<sup>o</sup>C
- Methane at 4<sup>o</sup>C

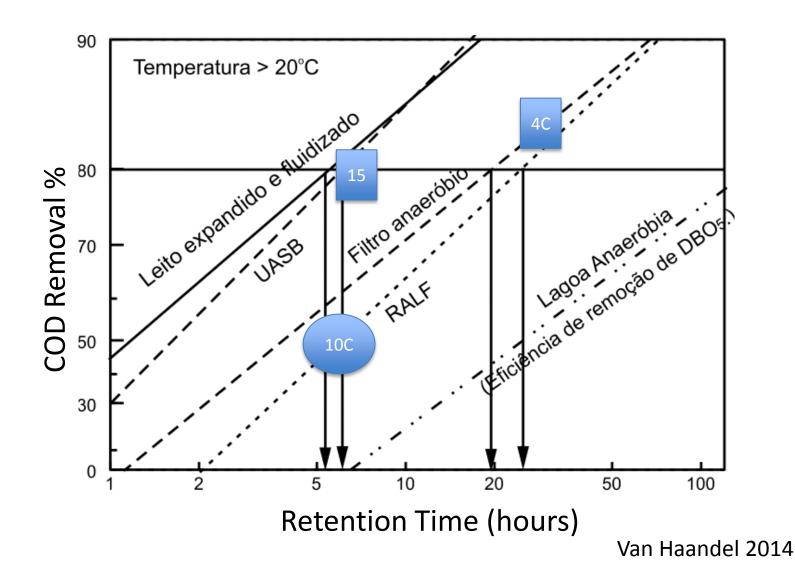


#### Sizing a reactor

Temperature °C	COD Turnover (fg/cell/day)	No. of Cells for Hydrolysis 100g COD	Reactor (m <sup>3</sup> /person)
4	76	$1.32 \times 10^{15}$	0.132
8	186	5.38×10 <sup>14</sup>	0.0538
15	250	$4.00 \times 10^{14}$	0.04

Temperature °C	CH₄ Turnover (fg/cell/day)	No. of Cells for Methanogenesis of 100g COD	Reactor (m <sup>3</sup> /person)
4	6.3	$1.32 \times 10^{15}$	0.254
8	7.6	$5.38 \times 10^{14}$	0.211
15	10.25	$4.00 \times 10^{14}$	0.156

#### Are we there yet?



### Get out of sludge!

- If you have O<sub>2</sub> you have sludge
  - "Yen canna break the laws of physics"
- Microbial Electrolysis Cells
  - "Works" at low temp
  - Not yet economic
- Anaerobic Domestic Wastewater
  - Can be done
  - Temperature problem close to solution

#### Anaerobic Domestic Wastewater Treatment

#### Thank You

#### My Colleagues in Newcastle

